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Our Ref: 11530/JAB/TCB
Date: 3rd December 2010
Status: Release 1 Final

Prepared for:
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DETERMINATION OF COMBUSTION PLANT FLUE GAS VELOCITY, VOLUMETRIC FLOW RATE AND GASEOUS EMISSIONS at FARMERS BOY (Deeside)

QUALITY REVIEW AND APPROVAL RECORD

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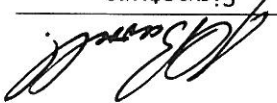
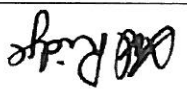
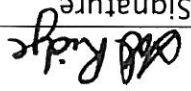
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Customer Name : Farmers Boy (Deeside) Ltd

Project No : 11530

Document Ref. No : 11530/JAB/TCB

Document held at NIFES Altrincham Office

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Approved for Issue:		Signature	Name	Date
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INTRODUCTION

In order to complete an application for an IPPC permit to operate a Meat Processing operation at their Deeside production unit, Farmers Boy (Deeside) Limited contacted NIFES Consulting Group to determine the velocity and volumetric flow of flue gases, plus to measure the emissions of oxides of Nitrogen and Carbon Monoxide in two process and six boiler stacks.

The tests were subsequently carried out on the 19th November 2010.

The flue gas velocity was determined for the following stacks:-

- Steam Boiler 1
- Steam Boiler 2
- Hot Water Heater 1
- Hot Water Heater 2
- LTHW Boiler 1
- LTHW Boiler 2
- Roaster A
- Roaster B
- Smoker



SUMMARY

As a result of the tests carried out, the following flue gas velocities volumetric flows were determined:-

Velocity (m/s)	Volumetric Flow (m ³ /h)	Stack @ 0°C Conditions	Concentration @ 3% O ₂ , 0°C, dry			Mass Emissions	
			CO mg/m ³	NO _x mg/m ³	CO g/h	NO _x g/h	
		12.1	5464	2851	13	157	29
		357					
Steam Boiler 1		7.3	2524	1438	15	117	18
Steam Boiler 2		4.2	743	537	1	396	1
Hot Water Heater 1		5.6	982	764	23	267	3
Hot Water Heater 2		1.8	115	63	84	225	3
Office Boiler 1		3.6	101	58	22	135	1
Office Boiler 2		<1.5	<330	<230	1744	<1	<9
Roaster 1		<1.5	281	<172	675	<1	<3
Roaster 2		<1.4	<154	<128	2813	<1	<8
Smoker							<1

Note: The above flue gas velocities and volumetric flows are quoted at the stack conditions existing at the time of the test, but will vary with firing rate and combustion conditions.

Pollutant concentrations are shown at the normally applied reference conditions for gas fired boilers.

In the case of smokers and roasters, no flue gas flows could be measured in the exhaust stack, although high flue gas temperatures indicated the plant was operational.

The high concentration of carbon monoxide indicated for the roasters and smoker reflects the high oxygen levels detected in the flue and the correspondingly large correction factor required to report the emissions at 3% oxygen. The actual concentrations at stack conditions is shown in Section 4.0.

Based on the above figures, emission from the cookers and, to a large extent, the office boilers can be largely discounted when considered in relation to the process plant.



1.0	METHODOLOGY	
1.1	Sample Position	All sampling was carried out at sample points provided by Farmers Boy (Deeside) Ltd personnel on the advice of NIFES' Engineer.
1.2	Velocity	The positions selected were chosen with a view to them providing a flat flow profile across the duct which would allow representative measurements to be taken. The position was however subject to limitations imposed by access to the test position.
1.3	Stack Temperature	Where possible, flue gas velocity was determined by carrying out a ten point traverse across each of the ducts using an NPL pitot tube in conjunction with an electronic micromanometer.
1.4	Stack Gas Concentration	Flue gas temperatures were measured using a K-type thermocouple and electronic temperature indicator.
1.5	Stack Area	The flue gas composition was determined using an ECOM SC Plus combustion analyser which measured oxygen, carbon monoxide, nitrogen oxide and nitrogen dioxide. The cross sectional area of the duct was derived from the diameter of the duct at the sample point.



Details of the test measurement are included in Appendix 1, but the figures derived are summarised below:-

2.0	TEST RESULTS
2.1	Steam Boiler No.2 (DEE 254)
2.2	Steam Boiler No.2 (DEE 255)
2.3	Hot Water Heater 1 (DEE 280)
2.4	Hot Water Heater 2 (DEE 281)
2.5	Office LTHW Boiler No.1

Stack Diameter	400mm
Flue Gas Temperature	250 °C
Flue Gas Oxygen Content	3.4% O ₂
Flue Gas Velocity	12.1 m/s
Volumetric Flow @ Stack Conditions	5464 m ³ /h
Volumetric Flow @ 0°C	2851 m ³ /h

BIB, Beavor, 1881 kW	
Stack Diameter	350mm
Flue Gas Temperature	206 °C
Flue Gas Oxygen Content	5.5% O ₂
Flue Gas Velocity	7.3 m/s
Volumetric Flow @ Stack Conditions	2524 m ³ /h
Volumetric Flow @ 0°C	1438 m ³ /h

Babcock Wanson, 1500 LNH 10, 1679 kg/h	
Stack Diameter	250mm
Flue Gas Temperature	105 °C
Flue Gas Oxygen Content	16.9% O ₂
Flue Gas Velocity	4.2 m/s
Volumetric Flow @ Stack Conditions	743 m ³ /h
Volumetric Flow @ 0°C	537 m ³ /h

State, SCE 65-5009, 128 kW	
Stack Diameter	250mm
Flue Gas Temperature	78 °C
Flue Gas Oxygen Content	18.1% O ₂
Flue Gas Velocity	5.7 m/s
Volumetric Flow @ Stack Conditions	982 m ³ /h
Volumetric Flow @ 0°C	764 m ³ /h

State, SBE 80500 NEUK, 146 kW	
Stack Diameter	150mm
Flue Gas Temperature	230 °C
Flue Gas Oxygen Content	9.7% O ₂
Flue Gas Velocity	1.8 m/s
Volumetric Flow @ Stack Conditions	115 m ³ /h
Volumetric Flow @ 0°C	63 m ³ /h

Ideal Mexico Super 2	
Stack Diameter	150mm
Flue Gas Temperature	230 °C
Flue Gas Oxygen Content	9.7% O ₂
Flue Gas Velocity	1.8 m/s
Volumetric Flow @ Stack Conditions	115 m ³ /h
Volumetric Flow @ 0°C	63 m ³ /h



2.6 Office LTHW Boiler No.2

Worcesster 28i (Combi)
Stack Diameter 100mm
Flue Gas Temperature 200 °C
Flue Gas Oxygen Content 9.2% O₂
Flue Gas Velocity 3.6 m/s
Volumetric Flow @ Stack Conditions 101 m³/h
Volumetric Flow @ 0°C 58 m³/h

2.7

Roaster 1

Stack Diameter 280mm
Flue Gas Temperature 118 °C
Flue Gas Oxygen Content 20.6% O₂
Flue Gas Velocity <1.5 m/s
Volumetric Flow @ Stack Conditions <330 m³/h
Volumetric Flow @ 0°C <230 m³/h

2.8

Roaster 2

Stack Diameter 280mm
Flue Gas Temperature 172 °C
Flue Gas Oxygen Content 20.6% O₂
Flue Gas Velocity <1.6 m/s
Volumetric Flow @ Stack Conditions <352 m³/h
Volumetric Flow @ 0°C <216 m³/h

2.9

Smoker

Stack Diameter 250mm
Flue Gas Temperature 56 °C
Flue Gas Oxygen Content 20.4% O₂
Flue Gas Velocity <1.4 m/s
Volumetric Flow @ Stack Conditions <241 m³/h
Volumetric Flow @ 0°C <200 m³/h



3.0 THEORETICAL FLUE GAS VOLUME

In addition to the flue gas volumes derived from measurements taken during the site visit, the theoretical flue gas volumes were also derived for the steam boilers when operating at their maximum capacity.

3.1	Boiler 1 – BIB Beavor	Flue gas volumetric flow (@ 250 °C and 3.4% O ₂) Flue gas volumetric flow (@ 0 °C and 3.4% O ₂ dry) Flue gas volumetric flow (@ 0 °C and 0% O ₂ dry)	5299 m ³ /h 2324 m ³ /h 1948 m ³ /h
3.2	Boiler 2 – Babcock Wanson	Flue gas volumetric flow (@ 206 °C and 5.5% O ₂) Flue gas volumetric flow (@ 0 °C and 5.5% O ₂ dry) Flue gas volumetric flow (@ 0 °C and 0% O ₂ dry)	3034 m ³ /h 1481 m ³ /h 1093 m ³ /h
3.3	Hot Water Heater 1	Flue gas volumetric flow (@ 248 °C and 7.7% O ₂) Flue gas volumetric flow (@ 0 °C and 7.7% O ₂ dry) Flue gas volumetric flow (@ 0 °C and 0% O ₂ dry)	366 m ³ /h 168 m ³ /h 106 m ³ /h
3.4	Hot Water Heater 2	Flue gas volumetric flow (@ 184 °C and 10.4% O ₂) Flue gas volumetric flow (@ 0 °C and 10.4% O ₂ dry) Flue gas volumetric flow (@ 0 °C and 0% O ₂ dry)	448 m ³ /h 240 m ³ /h 121 m ³ /h
3.5	Office Boiler 1	Flue gas volumetric flow (@ 230 °C and 9.7% O ₂) Flue gas volumetric flow (@ 0 °C and 9.7% O ₂ dry) Flue gas volumetric flow (@ 0 °C and 0% O ₂ dry)	115 m ³ /h 56 m ³ /h 30 m ³ /h
3.6	Office Boiler 2	Flue gas volumetric flow (@ 200 °C and 9.2% O ₂) Flue gas volumetric flow (@ 0 °C and 9.2% O ₂ dry) Flue gas volumetric flow (@ 0 °C and 0% O ₂ dry)	101 m ³ /h 52 m ³ /h 29 m ³ /h

(200 °C and 9.2% O₂ are anticipated conditions)

(230 °C and 9.7% O₂ were as-found conditions)

(184 °C and 10.4% O₂ were as-found conditions)

(248 °C and 7.7% O₂ were as-found conditions)

(206 °C and 5.5% O₂ were as-found conditions)

(250 °C and 3.4% O₂ were as-found conditions)

Boiler 1 – BIB Beavor

Boiler 2 – Babcock Wanson

Hot Water Heater 1

Hot Water Heater 2

Office Boiler 1

Office Boiler 2



4.0 FLUE GAS EMISSIONS

All the stacks identified were tested to determine the concentrations of the following gases in the flue gas:-

- oxygen (O₂)
- carbon monoxide (CO)
- nitrogen monoxide (NO)
- nitrogen dioxide (NO₂)
- sulphur dioxide (SO_x)

In all instances, no sulphur dioxide was recorded and the emissions are not reported.

In the case of the nitrogen oxides (NO & NO₂), these are combined in this report and reported as NO_x (oxides of nitrogen). In all instances, the proportion of NO₂ detected is less than 5%.

Using the measured concentrations and the flue gas volumetric flow rates, a mass emission figure has been devised for the boiler load at the time of testing.

Flue Gas Concentration at Stack			Concentration @ 3% oxygen dry gas		Mass Emissions	
O ₂	CO	NO _x	CO	NO _x	CO	NO _x
%	ppm	ppm	mg/m ³	mg/m ³	g/h	g/h
Steam Boiler 1	3.4	10	75	13	154	13
Steam Boiler 2	5.5	10	4.9	13	100	15
Hot Water Heater 1	169	1	44	1	90	1
Hot Water Heater 2	18.1	3	21	4	43	23
Office Boiler 1	9.7	42	69	53	141	84
Office Boiler 2	9.2	12	43	15	88	23
Roaster 1	20.6	31	<1	39	<1	1744
Roaster 2	20.6	30	<1	38	<1	1688
Roaster 3	20.4	50	<1	63	<1	2813
						<1



APPENDIX 1 TEST RESULTS

11530 Farmers Boy (Deeside) Ltd

NIFES Consulting Group

SITE Famers Boy - Deeside

POINT BABCOCK WANSON

DUCT SHAPE ROUND

FLUE DIAMETER 0.35 m
FLUE AREA 0.10 m²

TEST CONDITION As Found - High Fire

STACK TEMPERATURE 206 C
STACK TEMPERATURE 479 K

FLUE GAS OXYGEN 5.5 %

STATIC PRESSURE 25 pA

PLANE POINT	PITOT READING (Pa)				AVE. PITOT	SQ RT PITOT
	in	out				
1	15	15	15	15	15	3.87
2	16	18	18	17	17	4.12
3	20	22	22	21	21	4.58
4	25	27	27	26	26	5.10
5	30	32	32	31	31	5.57
6	25	37	37	31	31	5.57
7	20	23	23	22	22	4.64
8	15	18	18	17	17	4.06
9	11	14	14	13	13	3.54
10	10	10	10	10	10	3.16

AVERAGE IN PLANE
AVERAGE OVERALL

STACK VELOCITY 7.29 m/s

VOLUME FLOW (AT STACK CONDITIONS) 0.70 m³/s
2524 m³/h

VOLUME FLOW (AT OC) 0.40 m³/s
1438 m³/h

SITE Famers Boy - Deeside

POINT

Hot Water Boiler 1

DUCT SHAPE

ROUND

FLUE DIAMETER

0.25 m
0.05 m²

TEST CONDITION

As Found

STACK TEMPERATURE

105 C
378 K

FLUE GAS OXYGEN

16.9 %

STATIC PRESSURE

30 pA

PLANE POINT	PITOT READING (Pa)		AVE. PITOT	SQ RT PITOT
	in	out		
1	5	6	6	2.38
2	7	7	7	2.65
3	7	7	7	2.65
4	10	11	10	3.21
5	10	11	10	3.21
6	9	10	10	3.11
7	9	10	10	3.11
8	8	9	8	2.89
9	8	9	8	2.89
10	7	7	7	2.65

AVERAGE IN PLANE
AVERAGE OVERALL

STACK VELOCITY

4.21 m/s

VOLUME FLOW
(AT STACK CONDITIONS)

0.21 m³/s
743 m³/h

VOLUME FLOW
(AT OC)

0.15 m³/s
537 m³/h

SITE Famers Boy - Deeside

POINT Hot Water Boiler 2

DUCT SHAPE ROUND

FLUE DIAMETER 0.25 m
FLUE AREA 0.05 m²

TEST CONDITION As Found

STACK TEMPERATURE 78 C
STACK TEMPERATURE 351 K

FLUE GAS OXYGEN 18.1 %

STATIC PRESSURE 30 pA

PLANE POINT	PITOT READING (Pa)		AVE. PITOT	SQ RT PITOT
	in	out		
1	14	14	14	3.74
2	14	14	14	3.74
3	18	14	16	3.97
4	18	18	18	4.18
5	21	18	19	4.39
6	18	18	18	4.18
7	18	14	16	3.97
8	14	14	14	3.74
9	14	14	14	3.74
10	14	14	14	3.74

AVERAGE IN PLANE
AVERAGE OVERALL

STACK VELOCITY 5.56 m/s

VOLUME FLOW (AT STACK CONDITIONS) 0.27 m³/s
982 m³/h

VOLUME FLOW (AT OC) 0.21 m³/s
764 m³/h

SITE Famers Boy - Deeside

POINT

Roaster 1

DUCT SHAPE

ROUND

FLUE DIAMETER

0.28 m

FLUE AREA

0.06 m²

TEST CONDITION

As Found

STACK TEMPERATURE

118 C

391 K

FLUE GAS OXYGEN

20.6 %

STATIC PRESSURE

10 pA

PLANE POINT	PITOT READING (Pa)				AVE. PITOT	SQ RT PITOT
	in		out			
1	1	1	1	1	1	<1
2	1	1	1	1	1	<1
3	<1	<1	<1	<1	<1	<1
4	<1	<1	<1	<1	<1	<1
5	<1	<1	<1	<1	<1	<1
6	<1	<1	<1	<1	<1	<1
7	<1	<1	<1	<1	<1	<1
8	<1	<1	<1	<1	<1	<1
9	1	1	1	1	1	<1
10	1	1	1	1	1	<1
AVERAGE IN PLANE						
>						
1.00						

AVERAGE IN PLANE
AVERAGE OVERALL

STACK VELOCITY

< 1.49 m/s

VOLUME FLOW
(AT STACK CONDITIONS)

< 0.09 m³/s
< 330 m³/h

VOLUME FLOW

< 0.06 m³/s
< 230 m³/h

(AT OC)

		mg/m ³ @ stack O ₂	mg/m ³ @3%	g/h
NOx	0	0	0	0
CO	31	39	1744	9

SITE Famers Boy - Deeside

POINT Roaster 2

DUCT SHAPE ROUND

FLUE DIAMETER 0.28 m
FLUE AREA 0.06 m²

TEST CONDITION As Found

STACK TEMPERATURE 172 C
STACK TEMPERATURE 445 K

FLUE GAS OXYGEN 20.6 %

STATIC PRESSURE 10 pA

PLANE POINT	PITOT READING (Pa)	AVE. PITOT	SQ RT PITOT
1	<1	<1	<1
2	<1	<1	<1
3	<1	<1	<1
4	<1	<1	<1
5	<1	<1	<1
6	<1	<1	<1
7	<1	<1	<1
8	<1	<1	<1
9	<1	<1	<1
10	<1	<1	<1
AVERAGE IN PLANE			
AVERAGE OVERALL			

STACK VELOCITY

< 1.59 m/s

VOLUME FLOW (AT STACK CONDITIONS)

< 0.10 m³/s
< 352 m³/h

VOLUME FLOW (AT OC)

< 0.06 m³/s
< 216 m³/h

NOx	CO	mg/m ³ @ stack	ppm	O ₂	mg/m ³ @3%	g/h
			0	30	38	1688
			0	0	0	8

SITE Famers Boy - Deeside

POINT smoker

DUCT SHAPE ROUND

FLUE DIAMETER 0.25 m
FLUE AREA 0.05 m²

TEST CONDITION As Found

STACK TEMPERATURE 56 C
STACK TEMPERATURE 329 K

FLUE GAS OXYGEN 20.4 %

STATIC PRESSURE 10 pA

PLANE POINT	PITOT READING (Pa)	AVE. PITOT	SQ RT PITOT
1	<1	<1	<1
2	<1	<1	<1
3	<1	<1	<1
4	<1	<1	<1
5	<1	<1	<1
6	<1	<1	<1
7	<1	<1	<1
8	<1	<1	<1
9	<1	<1	<1
10	<1	<1	<1
AVERAGE IN PLANE			
AVERAGE OVERALL			

STACK VELOCITY

< 1.37 m/s

VOLUME FLOW (AT STACK CONDITIONS)

< 0.07 m³/s
< 241 m³/h

VOLUME FLOW

< 0.06 m³/s
< 200 m³/h

(AT OC)

NOx	mg/m ³ @ stack	O ₂	mg/m ³ @3%	g/h
0	0	0	0.00	0
13	50	62.5	2812.50	13
CO				

APPENDIX 2 THEORETICAL FLUE GAS VOLUMES



FARMERS BOY LTD - DEESIDE

BOILER No1 (ref DEE 254)
MAKE BIB
MODEL BEEVOR
AGE 2001
BURNER Nuway
MODEL NGN 80 T 35 430
FUEL Nat. Gas
High Fire

From Steam
steam out put 6,700 lbs/h
Energy to Steam 2,991 kg/h
heatoutput 1.88 MW
efficiency (nominal) 80 %
Healinput 2.35 MW
From Burner
burner 2.351 MW(MJ/s)
cv gas 38 500 MJ/m3
gas flow 0.06 m3/s
flue gas volume/m3gas 10.87 m3/m3
0% OC, wet 219.86 m3/h
0% OC, dry 8.86 m3/m3

FLUE GAS CONDITIONS		FLUE GAS VOLUMES	
MOISTURE	TEMPERATURE	OXYGEN	
DRY	0	0	0.541
WET	0	0	0.66
WATER	0	0	0.12
DRY	0	0	0.65
WET	0	0	0.77
DRY	250	3.4	1.24
WET	250	3.4	1.47
DRY			1948
			2390
			2324
			2766
			4453
			5299

NOX	CO
ppm	g/h
stack O ₂	157.24
mg/m ³ @3	12.78
%	29

FARMERS BOY LTD - DEESIDE

BOILER No1 (ref DEE 254)
MAKE BIB
MODEL BEEVOR
AGE 2001
BURNER Nuway
MODEL NGN 80 T 35 430
FUEL Nat. Gas
Low fire

From Steam
steam out put 6,700 lbs/h
Energy to Steam 2,991 kg/h
heatoutput 1.88 MW
efficiency (nominal) 80 %
Healinput 2.35 MW
From Burner
burner 2.351 MW(MJ/s)
cv gas 38 500 MJ/m3
gas flow 0.06 m3/s
flue gas volume/m3gas 10.87 m3/m3
0% OC, wet 219.86 m3/h
0% OC, dry 8.86 m3/m3

FLUE GAS CONDITIONS		FLUE GAS VOLUMES	
MOISTURE	TEMPERATURE	OXYGEN	
DRY	0	0	0.541
WET	0	0	0.66
WATER	0	0	0.12
DRY	0	0	0.65
WET	0	0	0.77
DRY	200	11.2	2.01
WET	200	11.2	2.22
DRY			1948
			2390
			442
			4174
			4616
			7232
			7998

NOX	CO
ppm	g/h
stack O ₂	161.91
mg/m ³ @3	137.76
%	205
	174

BOILER
MAKE BABCOCK WANSON
MODEL 15 LNH 10
AGE n/a
BURNER Riello
MODEL RS 130
FUEL Nat. Gas
High Fire

From Steam

steam out put 3,760 lbs/h
1,679 kg/h
0.47 kg/s
2264 kJ/kg

heatoutput

efficiency (nominal) 80 %
1.32 MW

From Burner

burner 1.320 MW(MJ/s)
cv gas 38,500 MJ/m3
gas flow 0.03 m3/s
flue gas volume/m3gas 10.87 m3/m3
8.86 m3/m3

GasConditions

OXYGEN 5.5 %
TEMP 206 C

FLUE GAS CONDITIONS		FLUE GAS VOLUMES	
MOISTURE	TEMPERATURE	OXYGEN	m3/s
DRY	0	0	0.304
WET	0	0	0.37
WATER	0	0	0.07
DRY	0	5.5	0.41
WET	0	5.5	0.48
DRY	206	5.5	0.72
WET	206	5.5	0.84
DRY	206	5.5	1093
WET	206	5.5	1341
DRY	206	5.5	1729
WET	206	5.5	2599
DRY	206	5.5	3034

mg/m3@		mg/m3@3%	
stack O2	ppm	g/h	
49	100	103	149
10	13	13	19
CO			

BOILER
MAKE
MODEL
AGE
BURNER
FUEL

Water Heater (ref: DEE 280)
 State
 SCE 65-500 G
 N/A
 atmospheric
 Nat. Gas

GasConditions

heatoutput 0.100 MW
 efficiency 78 %
 Heatinput 0.128 MW
From Burner
 burner 0.128 MW(MJ/s)
 cv gas 38.5 MJ/m³
 gas flow 0.003 m³/s
 flue gas volume/m³gas 10.87 m³/m³
 8.86 m³/m³
 0%,0C,wet
 0%,0C,dry
 11.99 m³/h

TEMP 248 C
 OXYGEN 7.7 %

FLUE GAS CONDITIONS		TEMPERATURE		OXYGEN		FLUE GAS VOLUMES	
DRY	WET	DRY	WET	DRY	WET	m ³ /s	m ³ /h
0	0	0	0	0	0.030		106
0	0	0	0	0	0.04		130
0	0	0	0	0	0.01		24
0	0	0	0	0	0.05		168
0	0	0	0	0	0.05		192
0	0	0	0	0	0.09		320
248	248	7.7	7.7	0.10	0.10		366

NOx	CO
mg/m ³ @ stack O ₂	ppm
272.65	133
3.75	3
369.00	45.73
5.08	0.63
%	kg/h

NOx

BOILER
MAKE
MODEL
AGE
BURNER
FUEL

Water Heater (ref: DEE 280)
 State
 SCE 65-500 G
 N/A
 atmospheric
 Nat. Gas

GasConditions

heatoutput 0.100 MW

efficiency 78 %
 Heatinput 0.128 MW

From Burner

burner 0.128 MW(MJ/s)
 cv gas 38.5 MJ/m³
 gas flow 0.003 m³/s
 flue gas volume/m³gas 10.87 m³/m³
 8.86 m³/m³
 0%,0C,wet
 0%,0C,dry
 11.99 m³/h

TEMP 105 C
 OXYGEN 16.9 %

FLUE GAS CONDITIONS		TEMPERATURE		OXYGEN		FLUE GAS VOLUMES	
DRY	WET	DRY	WET	DRY	WET	m ³ /s	m ³ /h
0	0	0	0	0	0.030		106
0	0	0	0	0	0.04		130
0	0	0	0	0	0.01		24
0	0	0	0	0	0.05		544
0	0	0	0	0	0.16		568
0	0	0	0	0	0.21		753
105	105	16.9	16.9	0.22	0.22		787

NOx	CO
mg/m ³ @ stack O ₂	ppm
44	1
90	1
396	5
49	1
%	g/h

FLUE GAS CONDITIONS		TEMPERATURE		OXYGEN		FLUE GAS VOLUMES	
DRY	0	0	0	0.034	121		
WET	0	0	0	0.04	149		
WATER	0	0	0	0.01	27		
DRY	0	0	0	0.07	240		
WET	0	0	0	0.07	267		
DRY	184	10.4	0.11	0.12	402		
WET	184	10.4	0.11	0.12	448		

CO	NOx	mg/m3@ stack O2	ppm	% mg/m3@3	g/h
3	21	43.05	3	23.28	33

BOILER MAKE MODEL AGE BURNER FUEL
Office space heating Ideal Mexico Super 2 n/a atmospheric Nat. Gas

heatoutput 0.029 MW

efficiency 80 %

Heatinput 0.036 MW

From Burner

0.036 MW(MJ/s)

38.500 MJ/m³

0.001 m³/s

10.87 m³/m³

8.86 m³/m³

0%_{OC,wet} 0%_{OC,dry}
3.39 m³/h

flue gas volume/m³gas

gas flow

cv gas

burner

GasConditions

OXYGEN

9.7 %

TEMP

230 C

FLUE GAS CONDITIONS				FLUE GAS VOLUMES	
MOISTURE	TEMPERATURE	OXYGEN		m ³ /s	m ³ /h
DRY	0	0	0	0.008	30
WET	0	0	0	0.01	37
WATER	0	0	0	0.00	7
DRY	0	9.7	0.02	0.02	56
WET	0	9.7	0.02	0.03	63
DRY	230	9.7	0.03	0.03	103
WET	230	9.7	0.03	0.03	115

NOX		CO	
mg/m ³ @	ppm	mg/m ³ @	g/h
stack O ₂	69	225	7.89
53	42	84	2.93

BOILER
MAKE Worcester
MODEL 28i Junior (Combi)
AGE 2008
BURNER atmospheric
FUEL Nat. Gas

heatoutput 0.028 MW

efficiency 80 %

Heatinput 0.035 MW

From Burner

0.035 MW(MJ/s)

38.500 MJ/m3

0.001 m3/s

10.87 m3/m3

8.86 m3/m3

0%,0C,wet
 0%,0C,dry
 3.27 m3/h

flue gas volume/m3gas

gas flow

cv gas

burner

GasConditions

OXYGEN

9.2 %

TEMP

200 C

FLUE GAS CONDITIONS				FLUE GAS VOLUMES	
MOISTURE				m3/s	m3/h
TEMPERATURE					
OXYGEN					
DRY	0	0	0	0.008	29
WET	0	0	0	0.01	36
WATER	0	0	0	0.00	7
DRY	0	0	0	0.01	52
WET	0	0	0	0.02	58
DRY	0	0	0	0.02	89
DRY	200	9.2	0.03		101

mg/m3@				g/h	
stack O2					
ppm					
mg/m3@3%					
NOx	43	88.15	134.47		5
CO	12	15	22.88		1

