

Schedule 6 - Notification

These pages outline the information that the operator must provide.

Units of measurement used in information supplied under Part A and B requirements shall be appropriate to the circumstances of the emission. Where appropriate, a comparison should be made of actual emissions and authorised emission limits.

If any information is considered commercially confidential, it should be separated from non-confidential information, supplied on a separate sheet and accompanied by an application for commercial confidentiality under the provisions of the PPC Regulations.

Part A

Permit Number	EPR/DP3934EW (formerly ZP3331LP)
Name of operator	ENI UK Ltd. Liverpool Bay Asset
Location of Installation	Talacre Holywell Flintshire CH8 9RD
Time and date of the detection	14:03 03/11/2017

(a) Notification requirements for any malfunction, breakdown or failure of equipment or techniques, accident, or fugitive emission which has caused, is causing or may cause significant pollution	
To be notified within 24 hours of detection	
Date and time of the event	03/11/2017 14:03
Reference or description of the location of the event	POA Terminal - Thermal Oxidiser (TOX) CEMS
Description of where any release into the environment took place	Release is via TOX stack (Emission point reference – A1)
Substances(s) potentially released	Sulphur Dioxide (SO ₂) Nitrogen Oxide (NO _x)
Best estimate of the quantity or rate of release of substances	Hourly Average emission levels SO ₂ – 1500 mg/nm ³ Hourly Average emission levels NO _x – 45 mg/nm ³
Measures taken, or intended to be taken, to stop any emission	Monitored SRU process parameters. CCR Operator monitoring plant operating conditions.
Description of the failure or accident.	Following start-up of the POA facilities after the pipeline span remediation, operating pressure in the Airbox of the Reaction Furnace has been increasing gradually. Source of the backpressure include significant contamination of the contact condenser in the Tail gas unit with solids and Sulphur blockages in the 2nd and 3rd condenser. Blockages in the contact condenser have worsened in the last 12 hours, increase in the backpressure from 0.4 barg to 0.6 barg has been observed. POA operations have backflushed the contact condenser several times to clear the blockage and minimize the operating pressure but the blockage hasn't been resolved. Samples of the fluid still suggest significant presence of solids in the sample.

	<p>If the Tail gas unit is taken offline, it will reduce the operating pressure in the Sulphur Recovery Unit and will help to flush the contact condenser from top to bottom in the Caustic sump. Multiple top to bottom flushes with steam condensate will help to resolve the current issues encountered with significant contamination of the fluids and provide higher reliability of Tail gas unit. Plan for resolving the contamination issues will be as follows;</p> <ul style="list-style-type: none"> · TGU wet section from Contact condenser will be bypassed and the tail gas from the downstream of the Reducing Gas Generator will be diverted to the Thermal Oxidiser (TOX). RGG will remain online to allow a quicker turnaround of TGU. · Once the Caustic sump is emptied by Veolia Tanker this afternoon, Contact Condenser will be flushed from top to bottom. Strainers on the pump suction will be taken out for clearing. Sample will be collected to ascertain the level of contamination in the system. · Next flushing activity will be carried out on Monday i.e. when the tanker is available again to take away the Spent Caustic sump/fluids retrieved from the column. · Once the results of the sample taken after the flushing activity confirm that the contamination has reduced to acceptable levels, the wet section will be put back into service and the gases will be diverted again to the TOX via the TGU. <p>The offline duration is expected to be a week considering the availability of the tankers, the flushing activity duration and the start-up of the TGU Amine section</p>
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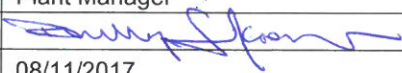
(b) Notification requirements for the breach of a limit	
To be notified within 24 hours of detection unless otherwise specified below	
Emission point reference/ source	A1 Thermal oxidizer
Parameter(s)	SO ₂ Hourly Average
Limit	190 mg/nm ³
Measured value and uncertainty	1500 mg/nm ³ +/- 300 mg/nm ³
Date and time of monitoring	Continuous Monitoring System
Measures taken, or intended to be taken, to stop the emission	Stabilize the Sulphur Recovery Unit and commence flushing operations on the Tail Gas Unit Contact Condenser

Time periods for notification following detection of a breach of a limit	
Parameter	Notification period
-	
-	
-	

(c) Notification requirements for the detection of any significant adverse environmental effect	
To be notified within 24 hours of detection	
Description of where the effect on the environment was detected	-
Substances(s) detected	-
Concentrations of substances detected	-
Date of monitoring/sampling	-

Part B - to be submitted as soon as practicable

Any more accurate information on the matters for notification under Part A.	
Measures taken, or intended to be taken, to prevent a recurrence of the incident	
Measures taken, or intended to be taken, to rectify, limit or prevent any pollution of the environment which has been or may be caused by the emission	
The dates of any unauthorised emissions from the installation in the preceding 24 months.	

Name*	Dhillip Sankoomar
Post	Plant Manager
Signature	
Date	08/11/2017 E-mail submission completed by Ela Kudlacik, ENI HSE Regulatory Advisor on 3 rd November 2017

* authorised to sign on behalf of ENI UK Ltd. Liverpool Bay Asset